## NATIONAL UNIVERSITY OF SCIENCE AND TECHNOLOGY

## FACULTY OF INDUSTRIAL TECHNOLOGY BACHELOR OF ENGINEERING (HONS) DEGREE Part Two Examination May 2014

## **TCE 2004 Chemical Engineering Thermodynamics**

Duration of Examination 3 Hours

Instructions to Candidates

- 1. Answer **Question One** and any other **Three** questions.
- 2. Show all your steps clearly in your calculation.
- 3. Start the answers for each question on a new page.
- 1. a) Estimate V, U, H and S for 1-butene vapour at 200°C and 70 bar if H and S are set equal to zero for saturated liquid at 0°C. Assume that the only data available are :  $T_c = 420 \text{ K}$   $P_c = 40.43 \text{ bar}$   $\omega = 0.191$   $T_n = 266.9 \text{ K}$  $Cp^{ig}/R = 1.967 + 31.630 \times 10^{-3} \text{ T} - 9.837 \times 10^{-6} \text{ T}^2$  [15]

b) Consider the steady-state adiabatic, irreversible flow of an incompressible liquid in a horizontal pipe of constant cross-sectional area. Show that:

- i) the velocity is constant [2]
- ii) the temperature increases with direction of flow [3]

c) Explain how flow in pipes differs from that in nozzles clearly, showing which case is more advantageous and why? [5]

a) Discuss the practical applications of exact differentials and partial derivatives in the study of thermodynamic properties of fluids. [6]

b) A 1.5m<sup>3</sup> tank contains 500kg of liquid water in equilibrium with pure water vapour, which fills the remainder of the tank. The temperature and pressure are 100°C and 101.33kPa. From a water line at constant temperature of 70°C and a constant pressure of somewhat above 101.33kPa, 750kg of liquid is bled into the tank. If the temperature and Page 1 of 3

pressure in the tank do not change as a result of the process, how much energy, as heat, must be transferred to the tank? [9]

c) Analyse the two main reasons for inaccuracy in the calculation of thermodynamic properties for the construction of a table or diagram. [4]

d) With the aid of equations define fugacity outlining its importance and how it differs for an ideal gas mixture, ideal solution of gas and real gas mixture. [6]

- 3. a) Compare and contrast excess properties and residual properties in the study of thermodynamic properties of fluids. [6]
  - b) Show from first principles that:

$$\frac{V}{(i)} \frac{V}{RT} = \left[\frac{\partial (G/RT)}{\partial F}\right] T$$

$$\frac{H}{R} = \pi \left[\frac{\partial (C/RT)}{\partial F}\right]$$
[5]

(ii) 
$$\overline{RT} = -I \begin{bmatrix} \partial T \end{bmatrix} P$$
 [5]

c) State the fundamental property relation equations. [4]

d) A high velocity nozzle is designed to operate with steam at 700kPa and 300°C. At the nozzle inlet velocity is 30m/s. Calculate values of the ratio  $A/A_1$  (where  $A_1$  is the cross-sectional area of the nozzle inlet) for the section where pressure is 600, 500 and 400kPa. Assume that the nozzle operates isentropically. [5]

4. a) Determine the enthalpy and entropy changes of liquid water for a change of state from 1 bar and 25°C to 1000 bar and 50°C. The following data for water are available.

[10]

T /°C	P/ bar	$C_p / J mol^{-1} K^{-1}$	V /cm <sup>3</sup> mol <sup>-1</sup>	$\beta/K^{-1}$
25	1	75.305	18.071	256×10 <sup>-6</sup>
25	1000		18.012	366×10 <sup>-6</sup>
50	1	75.314	18.234	458×10 <sup>-6</sup>
50	1000		18.174	568×10 <sup>-6</sup>

b) State and explain the advantages and draw backs of using thermodynamic tables.[5]

c) Using data from steam tables:

(i) Determine the numerical values of  $G^{L}$  and  $G^{v}$  for saturated liquid and vapour at 1000kPa. [5]

(ii) Determine the numerical values of  $\Delta H^{lv}/T$  and  $\Delta S^{lv}$  at 1000kPa. [5]

5. a) Water at 45°C and 10kPa enters an adiabatic pump and is discharged at a pressure of 8 600kPa. Assume the pump efficiency to be 0.75. Calculate the work of the pump, the temperature change of the water, and the entropy change of the water. [8]

**<u>Data</u>** (saturated liquid water at 45°C)

 $V = 1.010 \text{ cm}^3/\text{kg}$   $\beta = 425 \times 10^{-6}$   $C_p = 4.178 \text{kJ/kgK}$ 

b) Some expressions for  $G^{E}/RT$  are incapable of representing LLE. An example is the Wilson equation: [5]

 $G^{E}/RT = -x_{1}ln(x_{1}+x_{2}\Lambda_{12}) - x_{2}ln(x_{2}+x_{1}\Lambda_{21})$ 

Show that the stability criteria are satisfied for all values of  $\Lambda_{12}$ ,  $\Lambda_{21}$  and  $x_1$ .

c) Define the tem partial molar property and clearly show its application in the practical field of chemical engineering. [5]

d) Justify the notion that the Gibbs energy, Helmholtz energy and partition function serve as generating functions for other thermodynamic properties. Include all the relevant equations in your justification. [7]

## END OF EXAM