

NATIONAL UNIVERSITY OF SCIENCE AND TECHNOLOGY

FACULTY OF INDUSTRIAL TECHNOLOGY
DEPARTMENT OF CHEMICAL ENGINEERING
BACHELOR OF ENGINEERING (HONS) DEGREE
Part Two Examination January 2011

Transport Phenomena-TCE 2101

Duration of Examination: 3 Hours

Instructions to Candidates

1. Answer question **ONE** and any other **THREE** questions
 2. Each question carries 25 marks
 3. Show all steps clearly in any calculation
 4. Start the answers for each question on a fresh page
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Question One

(a) State the equation for momentum diffusivity and thermal diffusivity. Give the names and units of the parameters. **(4 marks)**

(b) State the equation for the Sc and Pr numbers. Give the names and units of the parameters. **(4 marks)**

(c) Estimate the liquid mass diffusivity of propanol in a dilute solution of water at 15°C. **(4 marks)**

Data: $V_c = 14.8 \text{ cm}^3/\text{mol}$ $V_H = 3.7 \text{ cm}^3/\text{mol}$ $V_o = 7.4 \text{ cm}^3/\text{mol}$

(d) State the two equations used to evaluate gas mass diffusivity and one that is used evaluate liquid mass diffusivity clearly defining each term and giving the appropriate units. **(13 marks)**

Question Two

(a) State the Wilke and Chang equation and contrast its application with the Fuller and Hirschfelder equations. **(3 marks)**

(b) Give a schematic representation of diffusion with a crystal and explain each process in detail. **(7 marks)**

(c) The mass transfer co-efficient for a turbulent boundary layer formed over a flat plate has been correlated in terms of the local Nusselt number by

$$Nu_x = 0.029 Re_x^{4/5} Sc^{1/3}$$

Where x is the distance from the leading edge of the flat plate, the transition from laminar to turbulent flow occurs at $Re_x = 3 \times 10^5$. Develop an expression for the mean mass transfer coefficient for a flat plate of length L . **(15 marks)**

Data

$$k_{c,lam} = 0.332(D_{AB}/x)(Re_x)^{1/2}(Sc)^{1/3}$$

$$k_{c,turb} = 0.0292(D_{AB}/x)(Re_x)^{4/5}(Sc)^{1/3}$$

k_c average = integral of the sum of $k_{c,lam}$ and $k_{c,turb}$ all divided by L with limits of 0 to L_t and L_t to L respectively.

Question three

(a) Show clearly the derivation of the following analogies: - Chilton-Colburn, Prandtl and Reynold. Each correct stage carries marks. **(15 marks)**

(b) A beaker of ethyl alcohol was accidentally upset covering the top smooth surface of a laboratory bench. The exhaust fan in the laboratory hood produced a 6m/s air flow parallel to the surface, flowing across a 1m wide bench. The air was maintained at 289K and 1 atm (1.013×10^5 kPa). The vapour pressure of ethyl alcohol at 289K is 4000Pa. Determine the amount of alcohol evaporating from 1 square meter surface area each 60sec. **(10marks)**

Data

$$v = 1.48 \times 10^{-5} \text{ m}^2/\text{s} \quad D_{AB} = 1.26 \times 10^{-5} \text{ m}^2/\text{s} @ 289\text{K}$$

$$R = 8.314 \text{ Pa.m}^3/\text{mol.K} \quad W_A = k_c A (C_{A,S} - C_{A,\infty})$$

Question Four

(a) Define molecular diffusion and briefly explain its significance in mass transfer. **(2 marks)**

(b) Determine the diffusivity of carbon monoxide through a gas mixture in which the mole fractions are: **(5 marks)**

$$y_{O_2} = 0.25$$

$$y_{N_2} = 0.71$$

$$y_{CO} = 0.04$$

Data: $D_{CO-O_2} = 0.185 \times 10^{-4} \text{ m}^2/\text{s}$ at 273K, 1 atm
 $D_{CO-N_2} = 0.192 \times 10^{-4} \text{ m}^2/\text{s}$ at 288K, 1 atm

(c) State the mass transfer equivalent dimensionless number of the Nu number. Give the equation, names and units of the parameters. **(3 marks)**

(d) Show clearly, from first principle, that $1/K_L = 1/mk_G + 1/k_L$ and $1/K_G = 1/k_G + m/k_L$ and explain in detail the physical significance of each term. **(13 marks)**

(e) Clearly explain the physical significance of $1/K_L$ and $1/K_G$. **(2 marks)**

Question Five

In an experimental study of absorption of NH_3 by water in a wetted wall column, the value of K_G was found to be $0.205 \text{ lb mole NH}_3/\text{hr ft}^2 \text{ atm}$. At one point in the column, the gas contained 8 mole percent NH_3 and the liquid phase concentration was $0.004 \text{ mole of NH}_3 \text{ per ft}^3 \text{ of solution}$. The temperature was 68° F , and total pressure was 1 atm . 85% of the total resistance to mass transfer was found to be in the gas phase. If Henry's constant at 68° F is $0.215 \text{ atm/ (lb mole NH}_3/\text{ ft}^3 \text{ of solution)}$, calculate the individual film coefficients and interfacial compositions. **(25 marks)**

All The Best!!!!!!!!!!!!!!!!!!!!!!!!!!!!!!!!!!!!